

Sixth Semester B.E. Degree Examination, Dec.2013/Jan.2014
Heat and Mass Transfer

Time: 3 hrs.

Max. Marks:100

Note: 1. Answer FIVE full questions, selecting at least TWO questions from each part.
2. Use of heat transfer data book is permitted.

PART – A

- 1 a. Explain briefly the mechanism of conduction, convection and radiation heat transfer. (06 Marks)
- b. With sketches, write down the mathematical representation of three commonly used different types of boundary conditions for one dimensional heat equation in rectangular coordinates. (08 Marks)
- c. A plate of thickness 'L' whose one side is insulated and the other side is maintained at a temperature T_1 is exchanging heat by convection to the surrounding area at a temperature T_2 , with atmospheric air being the outside medium. Write mathematical formulation for one dimensional, steady state heat transfer, without heat generation. (06 Marks)
- 2 a. An electric cable of 10mm diameter is to be laid in atmosphere at 20°C. The estimated surface temperature of the cable due to heat generation is 65°C. Find the maximum percentage increase in heat dissipation, when the wire is insulated with rubber having $K = 0.155 \text{ W/mK}$. Take $h = 8.5 \text{ W/m}^2\text{K}$. (06 Marks)
- b. Differentiate between the effectiveness and efficiency of fins. (04 Marks)
- c. In order to reduce the thermal resistance at the surface of a vertical plane wall (50 × 50cm), 100 pin fins (1 cm diameter, 10cm long) are attached. If the pin fins are made of copper having a thermal conductivity of 300 W/mK and the value of the surface heat transfer coefficient is 15 W/m²K, calculate the decrease in the thermal resistance. Also calculate the consequent increase in heat transfer rate from the wall if it is maintained at a temperature of 200°C and the surroundings are at 30°C. (10 Marks)
- 3 a. Show that the temperature distribution in a body during Newtonian heating or cooling is given by $\frac{T - T_a}{T_i - T_a} = \frac{\theta}{\theta_i} = \text{Exp}\left(\frac{-h A_s t}{\rho C V}\right)$. (06 Marks)
- b. The steel ball bearings ($K = 50 \text{ W/mK}$, $\alpha = 1.3 \times 10^{-5} \text{ m}^2/\text{sec}$), 40mm in diameter are heated to a temperature of 650°C. It is then quenched in a oil bath at 50°C, where the heat transfer coefficient is estimated to be 300 W/m²K. Calculate:
 - i) The time required for bearings to reach 200°C.
 - ii) The total amount of heat removed from a bearing during this time and
 - iii) The instantaneous heat transfer rate from the bearings, when they are first immersed in oil bath and when they reach 200°C. (14 Marks)
- 4 a. With reference to fluid flow over a flat plate, discuss the concept of velocity boundary and thermal boundary layer, with necessary sketches. (05 Marks)
- b. The exact expression for local Nusselt number for the laminar flow along a surface is given by $\text{Nu}_x = \frac{h_x x}{k} = 0.332 \text{ Re}_x^{1/2} \text{ Pr}^{1/3}$. Show that the average heat transfer coefficient from $x = 0$ to $x = L$ over the length 'L' of the surface is given by $2h_L$ where h_L is the local heat transfer coefficient at $x = L$. (05 Marks)

Important Note : 1. On completing your answers, compulsorily draw diagonal cross lines on the remaining blank pages.
 2. Any revealing of identification, appeal to evaluator and/or equations written eg. 42+8 = 50, will be treated as malpractice.

- c. A vertical plate 15cm high and 10cm wide is maintained at 140°C. Calculate the maximum heat dissipation rate from both the sides of the plates to air at 20°C. The radiation heat transfer coefficient is 9.0 W/m²K. For air at 80°C, take $\nu = 21.09 \times 10^{-6}$ m²/sec, $Pr = 0.692$, $k_f = 0.03$ W/mK. (10 Marks)

PART – B

- a. Explain the physical significance of i) Nusselt number; ii) Grashoff number. (04 Marks)
- b. Air at 2 atm and 200°C is heated as it flows at a velocity of 12 m/sec through a tube with a diameter of 3cm. A constant heat flux condition is maintained at the wall and the wall temperature is 20°C above the air temperature all along the length of the tube. Calculate:
 i) The heat transfer per unit length of tube.
 ii) The increase in bulk temperature of air over a 4m length of the tube.
 Take the following properties for air $Pr = 0.681$, $\mu = 2.57 \times 10^{-5}$ kg/ms, $K = 0.0386$ W/mK and $C_p = 1.025$ kJ/kg K. (10 Marks)
- c. Obtain a relationship between drag coefficient, c_m and heat transfer coefficient, h_m for the flow over a flat plate. (06 Marks)
- 6 a. Derive an expression for LMTD of a counter flow heat exchanger. State the assumptions made. (08 Marks)
- b. What is meant by the term fouling factor? How do you determine it? (04 Marks)
- c. Engine oil is to be cooled from 80°C to 50°C by using a single pass counter flow, concentric tube heat exchanger with cooling water available at 20°C. Water flows inside a tube with inner diameter of 2.5cm and at a rate of 0.08 kg/sec and oil flows through the annulus at the rate of 0.16 kg/sec. The heat transfer coefficient for the water side and oil side are respectively $h_w = 1000$ W/m²°C and $h_{oil} = 80$ W/m²°C. The fouling factors is $F_w = 0.00018$ m²°C/W on both the sides and the tube wall resistance is negligible. Calculate the tube length required. (08 Marks)
- 7 a. Sketch a pool boiling curve for water and explain briefly the various regimes in boiling heat transfer. (06 Marks)
- b. Define mass transfer coefficient. (02 Marks)
- c. A 12cm outside diameter and 2m long tube is used in a big condenser to condense the steam at 0.4 bar. Estimate the unit surface conductance i) in vertical position; ii) in horizontal position. Also find the amount of condensate formed per hour in both the cases.
 The saturation temperature of the steam = 74.5°C.
 Average wall temperature = 50°C.
 The properties of water film at average temperature of $\frac{75.4 + 50}{2} = 62.7^\circ\text{C}$ are given below
 $\rho = 982.2$ kg/m³, $h_f = 2480$ kJ/kg, $K = 0.65$ W/mK, $\mu = 0.47 \times 10^{-3}$ kg/ms. (12 Marks)
- 8 a. State and prove Wiens displacement law of radiation. (06 Marks)
- b. The temperature of a black surface 0.2m² in area is 540°C. Calculate:
 i) The total rate of energy emission.
 ii) The intensity of normal radiation.
 iii) The wavelength of maximum monochromatic emissive power. (06 Marks)
- c. Derive an expression for a radiation shape factor and show that it is a function of geometry only. (08 Marks)
